ATTACHMENT A

1. (Currently amended) A solid catalyst component for the polymerization of olefins comprising Mg, a titanium compound selected from titanium tetrahalides, or of formula $TiX_n(OR^1)_{4-n}$, wherein $0 \leq n \leq 3$, X is halogen, and R^1 is C_1-C_{10} hydrocarbon group, a halogen, and an electron donor compound (ED) selected from ethers, esters, amines, ketones, or nitriles, wherein a molar ratio Mg/Ti ranges from 7 to 120 ~~is higher than 5~~, and a molar ratio ED/Ti is higher than 3.5.

2. (Original) The solid catalyst component according to claim 1, in which the ED compound is selected from the group consisting of ethers, esters and ketones.

3. (Original) The solid catalyst component according to claim 2, in which the ED compound is selected from the C2-C20 aliphatic ethers.

4. (Original) The solid catalyst component according to claim 3, in which the ethers are cyclic ethers.

5. (Original) The solid catalyst component according to claim 4, in which the cyclic ethers have 3-5 carbon atoms.

6. (Original) The solid catalyst component according to claim 5, in which the cyclic ether is tetrahydrofurane.

7. (Previously presented) The solid catalyst component

according to claim 2, in which the ED compound is selected from alkyl esters of C1-C20 aliphatic carboxylic acids.

8. (Previously presented) The solid catalyst component according to claim 7, in which the alkyl esters are selected from C1-C4 alkyl esters of aliphatic mono carboxylic acids.

9. (Previously presented) The solid catalyst component according to claim 8, in which the alkyl ester is ethylacetate.

10. (Original) The solid catalyst component according to claim 1, in which the ED/Ti molar ratio ranges from 3.7 to 40.

11. (Previously presented) The solid catalyst component according to claim 10, in which the ED/Ti molar ratio ranges from 4.5 to 30.

12. (Cancelled)

13. (Original) The solid catalyst component according to claim 1, in which the Mg atoms derive from $MgCl_2$.

14. (Cancelled)

15. (Currently amended) A catalyst for the polymerization of olefins comprising a product obtained by contacting:

(a) a solid catalyst component comprising Mg, a titanium compound selected from titanium tetrahalides,

or of formula $TiX_n(OR^1)_{4-n}$, wherein $0 \leq n \leq 3$, X is halogen, and R^1 is C_1-C_{10} hydrocarbon group, a halogen, and an electron donor compound (ED) selected from ethers, esters, amines, ketones, or nitriles, wherein a molar ratio Mg/Ti ranges from 7 to 120 ~~is higher than 5~~, and a molar ratio ED/Ti is higher than 3.5;

(b) at least one aluminum alkyl compound and, optionally,

(c) an external electron donor compound.

16. (Original) The catalyst according to claim 15, in which the aluminum alkyl compound is an Al trialkyl.

17. (Original) The catalyst according to claim 15, in which the aluminum alkyl compound is an aluminum alkyl halide.

18. (Previously presented) The catalyst according to claim 15, in which the aluminum alkyl compound is a product obtained by mixing an aluminum trialkyl compound with an aluminumalkyl halide.

19. (Original) The catalyst according to claim 15, in which the external electron donor compound is a C2-C20 aliphatic ether.

20. (Previously presented) The catalyst according to claim 19, in which the aliphatic ether is tetrahydrofurane.

21. (Previously presented) The catalyst according to claim 15, in which the external electron donor compound

is a silicon compound of formula $R_a^5R_b^6Si(OR^7)_c$, where a is 0, b is 1, c is 3, R^6 is a branched alkyl or cycloalkyl group, optionally containing heteroatoms, and R^7 is methyl.

22. (Original) The catalyst according to claim 15, which is obtained by pre-contacting the components (a), (b) and optionally (c) for a period of time ranging from 0.1 to 120 minutes at a temperature ranging from 0 to 90°C.

23. (Original) The catalyst according to claim 22, in which the pre-contact is carried out of in the presence of small amounts of olefins, for a period of time ranging from 1 to 60 minutes, in a liquid diluent, at a temperature ranging from 20 to 70°C.

24. (Previously presented) The catalyst according to claim 15, which is pre-polymerized with at least one olefin of formula CH_2=CHR, where R is H or a C1-C10 hydrocarbon group, up to forming amounts of polymer from about 0.1 up to about 1000 g per gram of solid catalyst component (a).

25. (Previously presented) A process comprising (co)polymerizing olefins CH_2=CHR, wherein R is hydrogen or a hydrocarbon radical having 1-12 carbon atoms, carried out in the presence of a catalyst comprising a product obtained by contacting:

(a) a solid catalyst component comprising Mg, a titanium compound selected from titanium tetrahalides, or of formula $TiX_n(OR^1)_{4-n}$, wherein $0 \leq n \leq 3$, X is halogen, and R^1 is C_1-C_{10} hydrocarbon group, a halogen, and an electron donor compound (ED) selected from ethers,

esters, amines, ketones, or nitriles, wherein a molar ratio Mg/Ti ranges from 7 to 120 ~~is higher than 5~~, and a molar ratio ED/Ti is higher than 3.5;

(b) at least one aluminum alkyl compound and, optionally,

(c) an external electron donor compound.

26. (Original) The process according to claim 25, for the preparation of an ethylene/alpha olefin copolymer having a content of alpha olefin ranging from 0.1 to 20% by mol.

27. (Previously presented) The process according to claim 26, wherein the process is carried out in gas-phase.

28. (Previously presented) The process according to claim 27 further comprising the following steps:

(i) contacting the catalyst components (a), (b) and optionally (c) for a period of time ranging from 0.1 to 120 minutes, at a temperature ranging from 0 to 90°C; optionally

(ii) pre-polymerizing with at least one olefin of formula CH_2=CHR, where R is H or a C1-C10 hydrocarbon group, up to forming amounts of polymer from about 0.1 up to about 1000 g per gram of solid catalyst component (a); and

(iii) polymerizing in the gas-phase ethylene, or mixtures thereof with α-olefins CH_2=CHR in which R is a hydrocarbon radical having 1-10 carbon atoms, in at least one fluidized or mechanically stirred bed reactor, in the presence of a product formed in steps (i) or (ii).

29. (Previously presented) The solid catalyst component

according to claim 1, in which the Mg/Ti molar ratio ranges from 10 to 110.

30. (Previously presented) The solid catalyst component according to claim 1, in which the Mg/Ti molar ratio ranges from 15 to 100.

31. (New) The catalyst according to claim 15, in which the Mg/Ti molar ratio ranges from 10 to 110.

32. (New) The catalyst according to claim 15, in which the Mg/Ti molar ratio ranges from 15 to 100.

33. (New) The process according to claim 25, in which the Mg/Ti molar ratio ranges from 10 to 110.

34. (New) The process according to claim 25, in which the Mg/Ti molar ratio ranges from 15 to 100.